IN THE CLAIMS:

- 1 (Original) A metal oxide alkylation catalyst precursor composition comprising a pore former and a catalyst reagent.
- 2. (Original) The catalyst precursor composition of claim 1 wherein the pore former is present in an amount of between 0.01 and 5 percent by weight based upon the total weight of the catalyst reagent.
- 3. (Original) The catalyst precursor composition of claim 1, wherein the catalyst reagent comprises a magnesium reagent, an iron reagent or a combination comprising one of the foregoing.
- 4. (Original) The catalyst precursor composition of claim 3, wherein the magnesium reagent comprises magnesium hydroxide, magnesium nitrate, magnesium carbonate, magnesium sulphate, magnesium acetate, or a combination comprising one of the foregoing.
- 5. (Original) The catalyst precursor composition of claim 3, wherein the iron reagent comprises ferric nitrate, ferric sulfate, ferric chloride, ferrous nitrate, ferrous sulfate, ferrous chloride, or a combination comprising one of the foregoing.
- 6. (Original) The catalyst precursor composition of claim 1 wherein the pore former is selected from the group consisting of waxes and polysaccharides.
- 7. (Original) The catalyst precursor composition of claim 6, wherein the pore former comprises paraffin wax, polyethylene wax, microcrystalline wax, montan wax, or a combination comprising one of the foregoing.

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- (Original) The catalyst precursor composition of claim 6, wherein the 8. polysaccharide is selected from one or more of cellulose, carboxyl methyl cellulose, cellulose acetate, starch, and walnut powder.
- (Original) The catalyst precursor composition of claim 1, wherein the pore former 9. is selected from the group consisting of citric acid, polyethylene glycol, oxalic acid, and stearic acid.
- (Original) The catalyst precursor composition of claim 1, wherein the pore former 10. is selected from paraffin, polyethylene and mixtures thereof.
 - (Original) A catalyst made from the catalyst precursor composition of Claim 1. 11.
- (Original) The catalyst as claimed in claim 11, wherein the metal oxide alkylation 12. catalyst has a bimodal distribution of pores less than 400 Angstroms.
- (Original) The catalyst as claimed in claim 12, wherein the bimodal distribution of 13. pores has a first distribution of pores wherein the first distribution has an average pore diameter less than 100 angstroms and a second distribution of pores wherein the second distribution has an average diameter greater than 100 angstroms and less than 400 Angstroms.
- (Withdrawn) A method for preparing a metal oxide alkylation catalyst comprising 14. the steps of (a) combining a pore former with at least one catalyst reagent selected from the group consisting of magnesium reagents and iron reagents to form a catalyst precursor composition and (b) calcining the catalyst precursor composition to form a metal oxide alkylation catalyst wherein the metal oxide alkylation catalyst has pores with a diameter between 100 and 400 Angstroms.
- (Withdrawn) The method of claim 14, wherein in step (a) the pore former is 15. incorporated in an amount of between 0.01 and 5 percent by weight based upon the total weight of the catalyst reagent.

- 16. (Withdrawn) The method of claim 14, wherein the catalyst reagent is selected from at least one of magnesium reagents and iron reagents.
- 17. (Withdrawn) The method of claim 14, wherein the magnesium reagent is selected from magnesium hydroxide, magnesium nitrate, magnesium carbonate, magnesium sulphate and magnesium acetate.
- 18. (Withdrawn) The method of claim 14, wherein the iron reagent is selected from ferric nitrate, ferric sulfate, ferric chloride, ferrous nitrate, ferrous sulfate and ferrous chloride.
- 19. (Withdrawn) The method of claim 14, wherein the pore former is selected from the group consisting of waxes and polysaccharides.
- 20. (Withdrawn) The method of claim 19, wherein the wax is selected from one or more of paraffin wax, polyethylene wax, microcrystalline wax, and montan wax.
- 21. (Withdrawn) The method of claim 19, wherein the polysaccharide is selected from one or more of cellulose, carboxyl methyl cellulose, cellulose acetate, starch, and walnut powder.
- 22. (Withdrawn) The method of claim 19, wherein the pore former is selected from one or more of citric acid, polyethylene glycol, oxalic acid, and stearic acid.
- 23. (Withdrawn) The method of claim 14, wherein the pore former is selected from paraffin, polyethylene and mixtures thereof.
- 24. (Withdrawn) The method of claim 14, wherein the pore former is present in an amount effective to result in pores having a diameter between 100 and 200 angstroms after the catalyst precursor composition has been subjected to calcination.
- 25. (Withdrawn) The method of claim 14, wherein the calcination is done under a flow of gas with a weight hourly space velocity of between about 0.01 to 0.25.

- 26. (Withdrawn) The method of claim 25, wherein the gas is selected from oxygen, nitrogen, air and mixtures thereof.
- 27. (Withdrawn) The method of claim 14, wherein the calcination is effected at a temperature between 350 and 600°C.
- 28. (Withdrawn) The method of claim 14, wherein the metal oxide alkylation catalyst has a bimodal distribution of pores less than 400 Angstroms.
- 29. (Withdrawn) The method of claim 14, wherein the bimodal distribution of pores has a first distribution of pores wherein the first distribution has an average pore diameter less than 100 angstroms and a second distribution of pores wherein the second distribution has an average diameter greater than 100 angstroms and less than 400 Angstroms.

30-34 (Cancelled)